

ENVIRONMENTAL FOOTPRINT COMPARISON TOOL

A tool for understanding environmental decisions related to the pulp and paper industry



EFFECTS OF DECREASED RELEASE OF CHLORINATED COMPOUNDS ON ENERGY USE

Importance of Unbleached Pulp Lignin Content

Kappa number is a measure of the amount of lignin remaining in pulp. The higher the kappa number value, the higher the use of bleaching chemicals required to brighten the pulp.

The kappa numbers of pulps leaving the digester are typically about 30 for softwoods and 20 for hardwoods in bleached kraft mills that employ conventional cooking methods. Several modifications to conventional cooking, known collectively as extended cooking (EC), have enabled kappa numbers to be further reduced in the digester in ways that minimize yield and strength losses. Kappa numbers associated with EC are about 20 for softwoods and about 14 for hardwoods.

Oxygen delignification (OD) is another technology that is used extensively to lower the residual lignin content prior to the bleach plant. The technology is more selective than most extended cooking processes. Lignin reductions of approximately 50% are achievable with OD, resulting in softwood kappa number in the 14-18 range.

Some mills use both extended cooking and oxygen delignification to achieve very low kappa number pulps prior to bleaching, producing pulps with kappa number values in the range of 10-12, perhaps even lower. Deterioration of pulp strength properties is the limiting obstacle for kappa number reduction prior to the bleach plant.

More recent strategies have been focused away from obtaining the most delignification possible in the digester and toward optimizing the fiberline as a whole based on economic, quality, and environmental factors. In these strategies, oxygen delignification plays a larger role because it can provide more selective lignin removal with less yield loss than extended cooking (Stratton, Gleadow, and Johnson 2005).

An EU appraisal of the kappa number reduction capabilities of the various pulping related technologies is summarized in Table C4.

Table C4. Kappa Numbers Currently Achieved after Different Technologies Used (Source: IPPC 2001)

| Delignification Technology | Hardwood | Softwood |
|---|----------|----------|
| Conventional Cooking | 14 - 22 | 30 - 35 |
| Conventional Cooking and Oxygen Delignification | 13 - 15 | 18 - 22 |
| Extended Cooking | 14 - 16 | 18 - 22 |
| Extended Cooking and Oxygen Delignification | 8 - 10 | 8 - 12 |

TCF bleaching requires a low incoming kappa number (10-12) for the pulp to attain full brightness and good strength properties because of the power of the bleaching chemicals and fiber degradation during bleaching. A final pulp brightness of 89% ISO is achievable with TCF bleaching without yield loss. A larger amount of residual lignin remains in TCF bleached pulp than in ECF bleached pulp and this residue has to be stabilized to minimize yellowing after production. ECF bleaching can be done on a pulp with a higher kappa number (IPPC 2001).

Effects of Decreased Release of Chlorinated Compounds on Energy Use
Importance of Unbleached Pulp Lignin Content

Data tabulated by Axegård et al. illustrates the significance of unbleached pulp kappa number to the electrical energy embodied in the production of bleaching agents.

Table C5. Approximate Costs and Use of Electrical Energy for Bleaching Chemicals Consumed in Different Bleaching Sequences (Source: Axegård et al. 2003)

| Post Oxygen Kappa Number | Bleaching Sequence | Bleaching Chemical Cost (USD/ptp) | Electrical Energy Requirements to Produce Bleaching Chemicals (ptp) ^a | |
|-----------------------------|-------------------------------|---|---|-----------|
| | | | kWh | kWh/Kappa |
| 18 | (C85+D15)(E ₀)DED | 22 | 160 | 9 |
| 18 | D(E _{PO})DD | 31 | 260 | 14 |
| 8 | D(E _{PO})DD | 22 | 150 | 19 |
| 8 | QPZP | 25 | 96 | 12 |

Based on laboratory bleaching of oxygen-delignified softwood kraft pulp bleached to ISO-brightness 90%.

^a Hydrogen peroxide is assumed to be generated from hydrogen produced by electrolysis of water.

The tabulation shows a 42% dividend in chemical energy accompanying the 55% kappa number reduction for a D(EPO)DD bleach sequence. The 36% energy reduction for the TCF sequence relative to the ECF sequence on the low kappa number pulp is also noteworthy.

References

- Axegård, P., J. Carey, J. Folke, P. Gleadow, J. Gullichsen, D. Pryke, D. Reeve, B. Swan, and V. Uloth. 2003. Minimum-impact mills: Issues and challenges. In *Environmental impacts of pulp and paper waste streams*, ed. T. Stuthridge, M.R. van den Hueval, N.A. Marvin, A.H. Slade, and J. Gifford. Pensacola, FL: SETAC Press.
- Integrated Pollution Prevention and Control (IPPC). 2001. *Reference document on best available techniques in the pulp and paper industry*. http://eippcb.jrc.ec.europa.eu/reference/BREF/ppm_bref_1201.pdf
- Stratton, S., Gleadow, P., and Johnson, A. 2005. Pulp mill process closure: A review of global technology developments and mill experiences in the 1990s. *Water Science & Technology* 50(3): 183-194.